

# Critical fouling conditions induced by colloidal surface interaction : from causes to consequences



## Causes :

property of concentrated colloidal suspension

## From causes to consequences :

a way to depict consequences of these properties on filtration

## Consequences :

critical filtered volume in dead end filtration

critical Pe number in cross flow filtration

structure and kinetics of deposit formation

## Critical flux : chronological account

### Before the critical flux birth

1986

- Colloid flux paradox (Cohen and Probstein 1986)
- Effect of colloid interaction of UF (McDonogh et al. 1989)
- In the review of Belfort, Davis and Zydney (1994)  
still exist a need to develop *“quantitative understanding of the possible interaction that can occur between particles in a complex process streams”*

### Critical flux : first definition

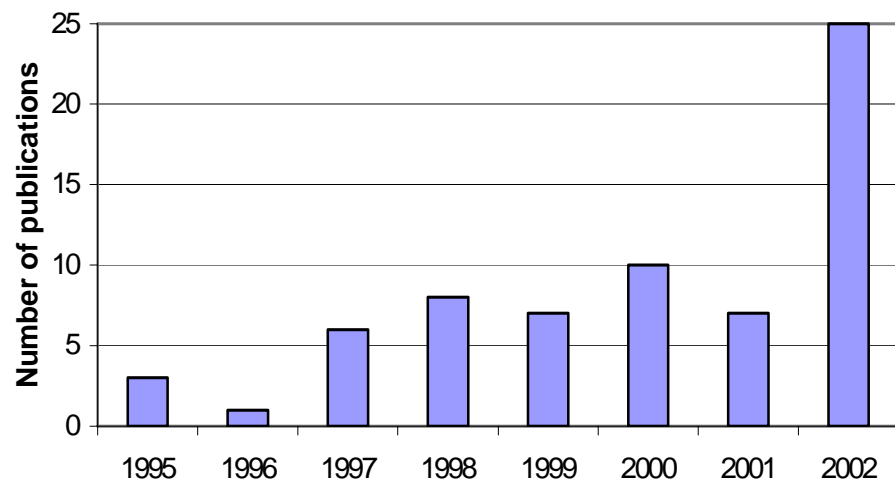
1995

- Theoretical demonstration and definition of critical flux (Bacchin 1994, 1995)  
*“flux required to overcome surface interaction and leads to coagulation at the membrane”*
- First experimental highlight (Field et al. 1995 and Howell 1995)  
Definition of *“sub critical flux operation”*

### Critical flux : evolution and importance of the concept

- In 2002, critical flux is used in around 10 % of publication dealing with membrane fouling (around 250 in a year)

2002



Causes

From causes to consequences

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## Surface interaction and concentration **control structure** of concentrated colloidal suspension

**Gas phase** : free and random move of particles in the solvent

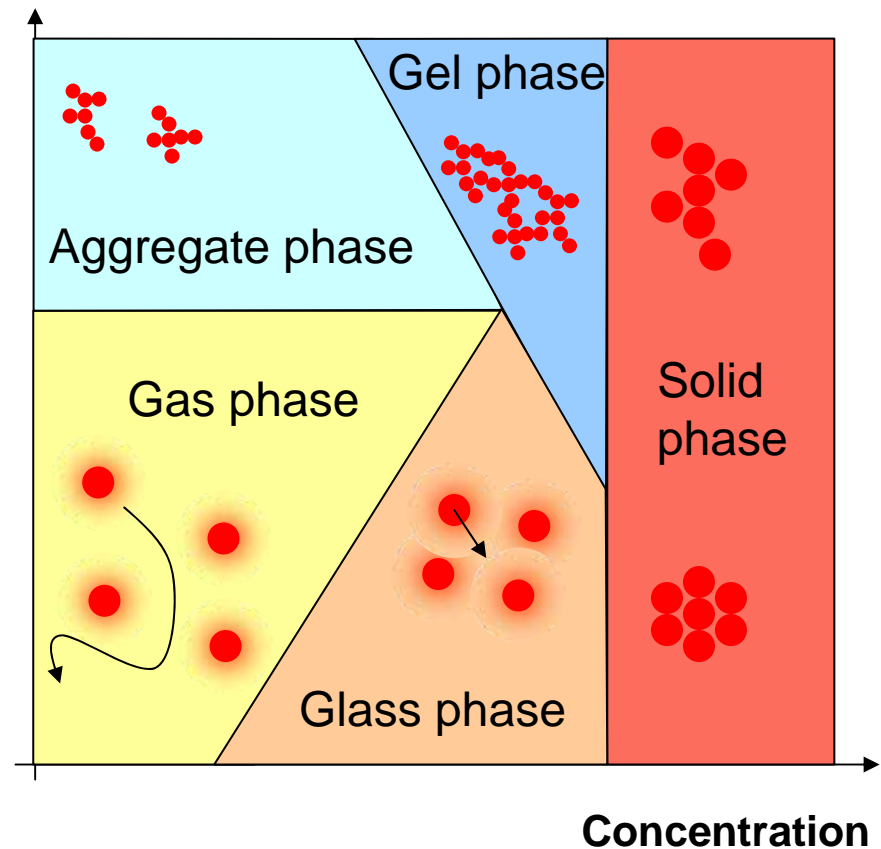
**Aggregate phase** : free and random Move of aggregates in the solvent

**Glass phase** : network of ordered repulsive particles (move from and towards equilibrium position)

**Gel phase** : network of elastic attractive particles

**Solid phase** : network of Particles in contact

destabilisation



Causes

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## Surface interaction and concentration **control phase transitions** in concentrated colloidal suspension

### Aggregation :

formation of aggregate

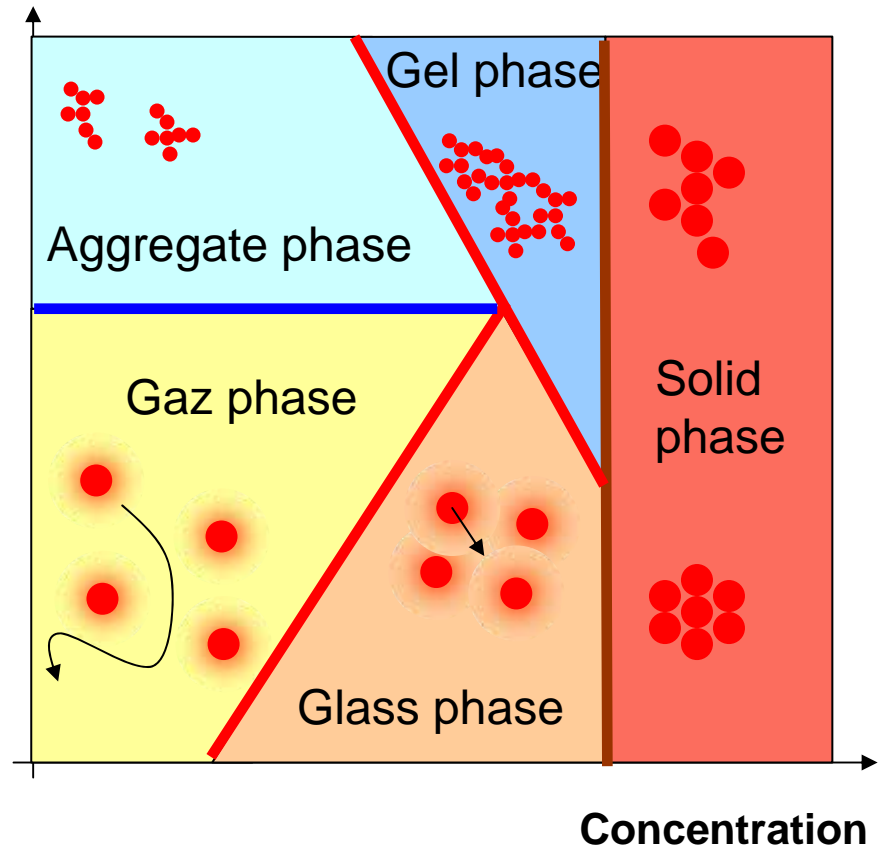
**Percolation** of attraction or repulsion : formation of a network

**Spinodal decomposition** :  
irreversible solid formation



**critical phenomena**  
in term of transition reversibility

destabilisation



Causes

From causes to consequences

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## Which properties can describe this complexity ?

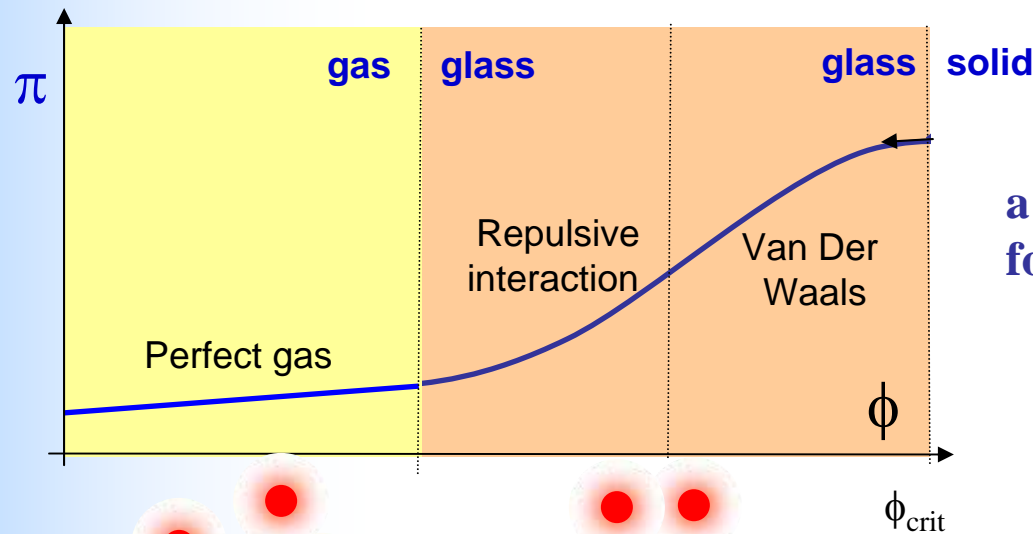
### Osmotic pressure, $\pi$ :

- relative to the resistance to the local over concentration of the suspension
- macroscopic property experimentally accessible
- relative to the equilibrium of the dispersed phase in the solvent sensitive to multi-body surface interaction and depicting phase transitions

relevant to filtration

measurable for complex fluid

adapted to describe the complexity responsible of fouling



a typical  $\pi$  curve for stable colloid

Causes

From causes to consequences

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## Osmotic pressure : a key property for filtration process

Osmosis

$$J = \frac{\Delta P - \pi_i}{\mu(R_m + R_c)}$$

Diffusion

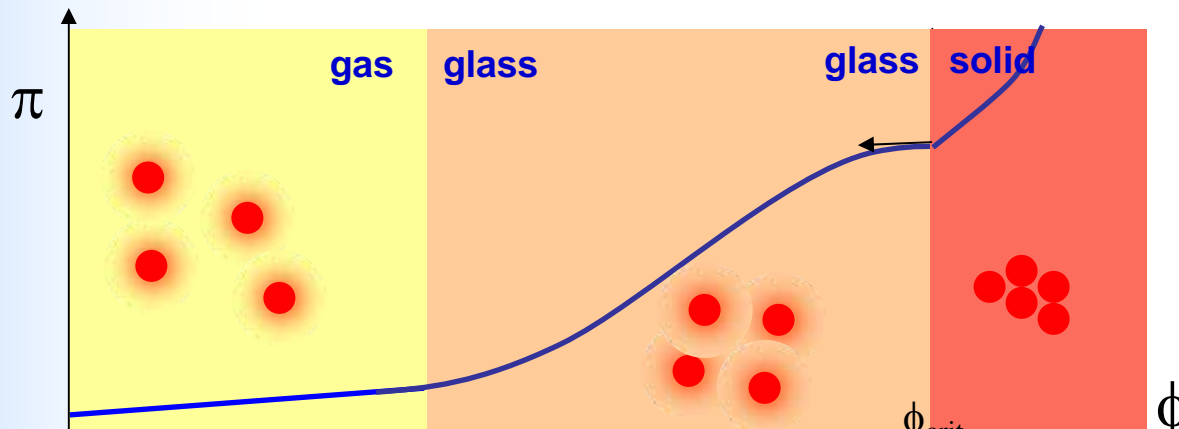
$$D(\phi) = \frac{K(\phi)}{6\pi\mu a} \frac{d\pi}{d\phi} V_p$$

+

**Compression yield :**  
resistance to the  
applied pressure in  
a deposit

**« Solid » pressure**

equation of state for the divided matter in water  
which describe continuously properties of colloidal suspension  
when concentrated from bulk to deposit



Causes

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## Analogy between diffusion in a polarised layer and permeation in a deposit using solid pressure

Mass balance in a polarised layer

$$J\phi - D(\phi)\frac{d\phi}{dx} = 0$$

Einstein [1] relation  
for diffusion coefficient

Permeation in a deposit

$$J = -\frac{k}{\mu} \frac{dp}{dx}$$

$$k = \frac{2a^2}{9} \frac{K(\phi)}{\phi} \quad [2]$$

$$\frac{d(p + \pi)}{dx} = 0 \quad [3]$$

A single equation to link  
accumulation to operating  
conditions and fluid properties

$$\phi dx = \frac{D_b}{J} K(\phi) d\pi^*$$

with  $\pi^* = \pi \frac{V_p}{k_B T}$

- [2] A.A. Zick and G.M. Homsy, Stokes flow through periodic arrays of spheres, *Journal of fluid mechanics*, 115 (1982) 13-26.
- [3] J.D. Sherwood, Initial and final stages of compressible filtercake compaction, *AIChE J.*, 43 (1997) 1488-1493.

Causes

From causes to consequences

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Solvent transfer

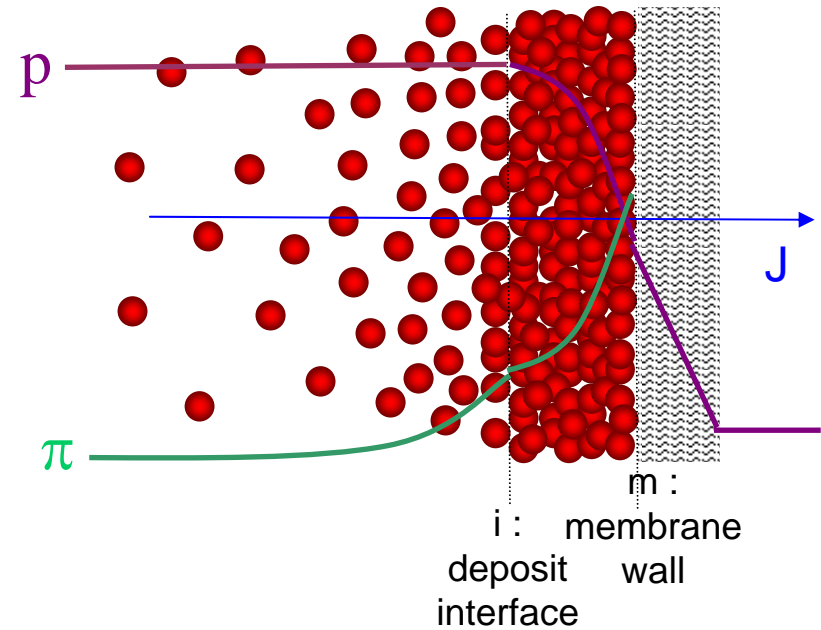
$$J = \frac{\Delta P - \pi_i}{\mu(R_m + R_c)}$$

●  $\frac{d(p + \pi)}{dx} = 0$

in the deposit

●  $J = \frac{p_i - p_m}{\mu R_c}$

➔  $\pi_m = \pi_{crit} + J\mu R_c$



Equation linking permeate flux to accumulation

$$\frac{J}{J_0} = 1 - \frac{\pi_m^*}{A}$$

with  $A = \frac{\Delta P V_p}{kT}$

●  $\pi_m < \pi_{crit}$  polarized layer

●  $\pi_m > \pi_{crit}$  polarized layer with  $\pi_i = \pi_{crit}$

and deposit with  $R_c = \frac{\pi_m - \pi_{crit}}{J\mu}$

« Solid » pressure can describe in a same equation both osmosis phenomenon and deposit resistance



## Causes

## From causes to consequences

## Consequences

**Dead end filtration :**  
accumulated volume  
fraction

$$Pe = \frac{JV_a}{D_b} = \int_{\pi_b^*}^{\pi_m^*} K(\phi) d\pi^*$$

$$V_a = \int_0^{\infty} \phi dx \quad \begin{array}{l} \text{volume} \\ \text{accumulated} \\ \text{per area} \end{array}$$

Pe number =  $\frac{\text{dissipated friction energy on whole particles accumulated}}{\text{Brownian energy}}$

integration of

$$\phi dx = \frac{D_b}{J} K(\phi) d\pi^*$$

**Cross flow filtration :**  
accumulation in a given  
boundary layer thickness

$$Pe = \frac{J\delta}{D_b} = \int_{\pi_b^*}^{\pi_m^*} \frac{K(\phi)}{\phi} d\pi^*$$

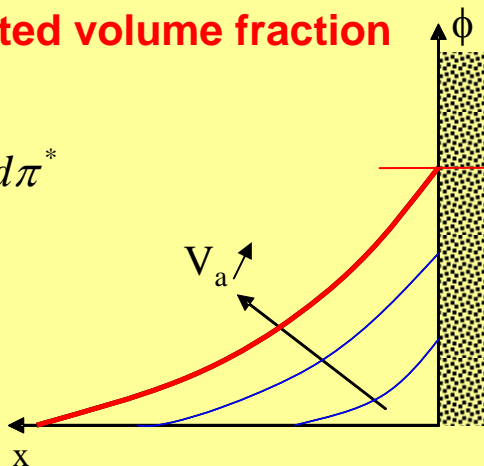
$$\delta = \int_0^{\delta} dx \quad \begin{array}{l} \text{length of mass} \\ \text{boundary} \\ \text{layer} \end{array}$$

Pe number =  $\frac{\text{dissipated friction energy on a particle across BL}}{\text{Brownian energy}}$

## Critical fouling conditions

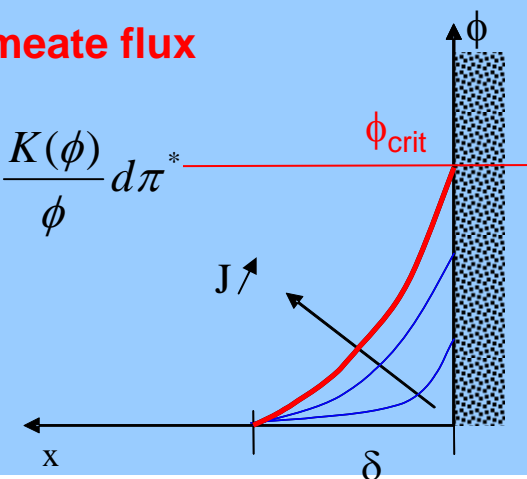
## Critical accumulated volume fraction

$$V_{a \text{ crit}} = \frac{D_b}{J} \int_{\pi_b^*}^{\pi_{crit}^*} K(\phi) d\pi^*$$



## Critical permeate flux

$$J_{crit} = \frac{D_b}{\delta} \int_{\pi_b^*}^{\pi_{crit}^*} \frac{K(\phi)}{\phi} d\pi^*$$



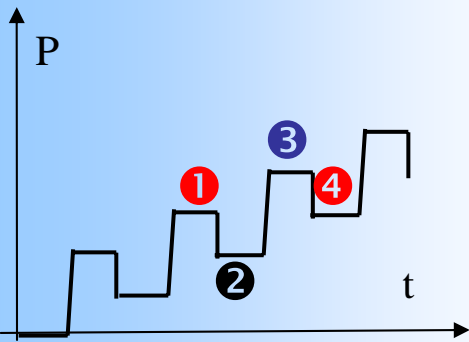
Causes

From causes to consequences

Consequences / Cross flow

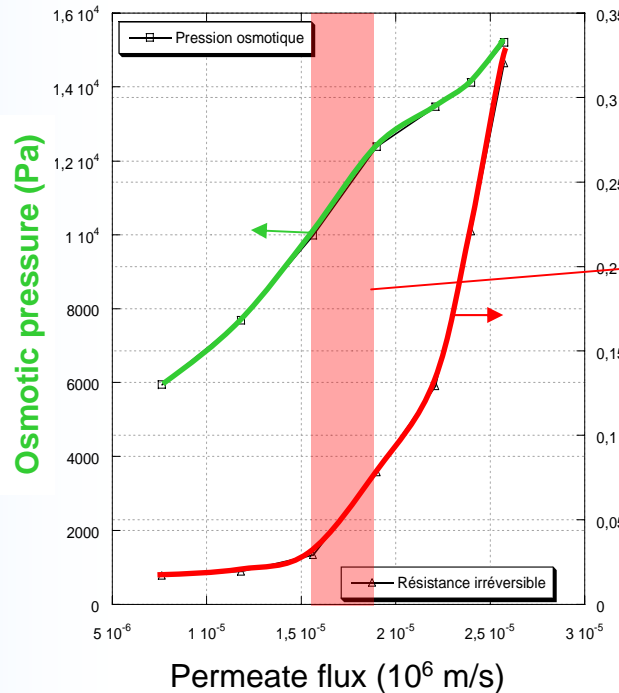
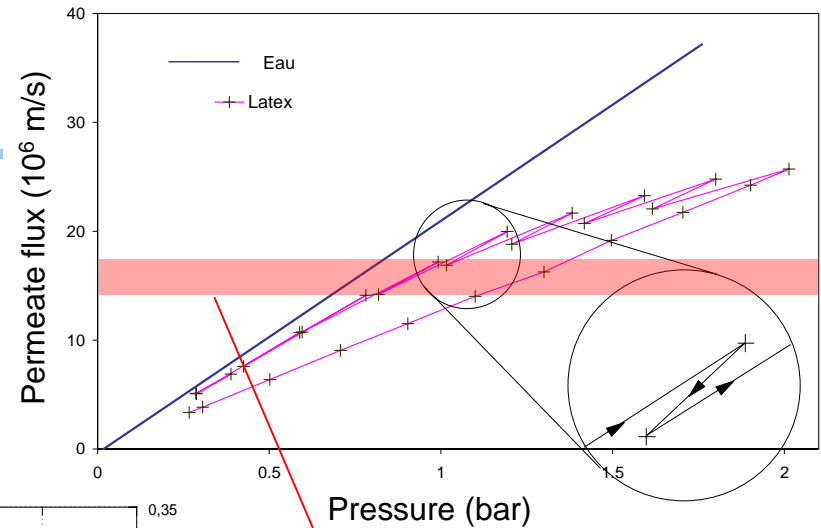
# Experimental determination of critical flux

## Principles



Fouling comparison in pressure step 1 and 4 allows determining the irreversibility degree of fouling in step 3

## Results



Deposit resistance over membrane resistance

**critical flux**

$J_{crit} = f(\text{colloidal interaction, hydrodynamics})$

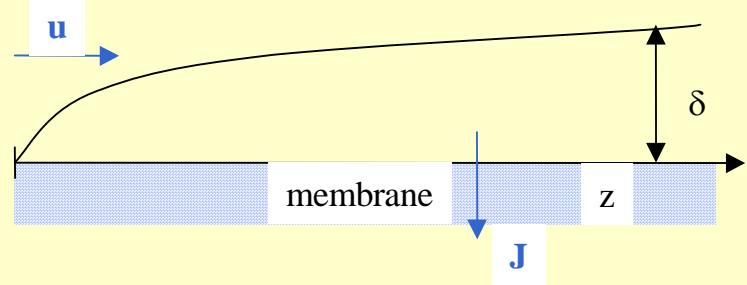
## Consequences of a critical Peclet number

**u** : cross flow velocity  
**z** : axial position

$$Pe_{crit} = \frac{J_{crit} \delta}{D} = \int_{\pi_b^*}^{\pi_{crit}^*} \frac{K(\phi)}{\phi} d\pi^*$$

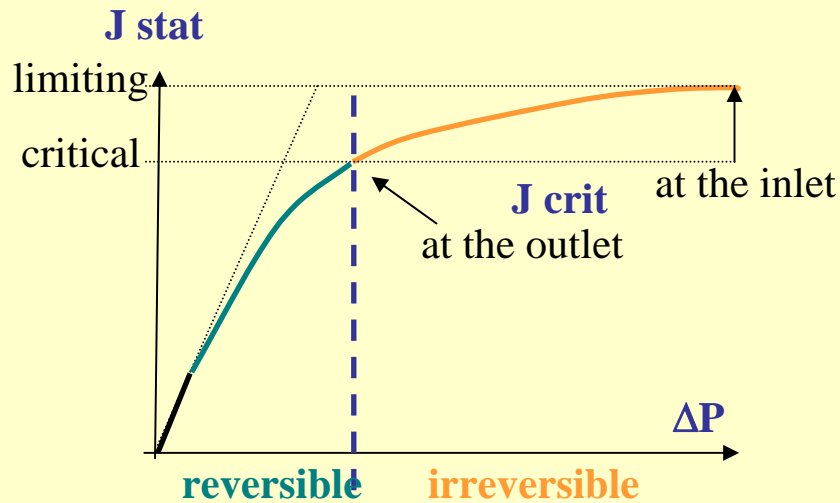
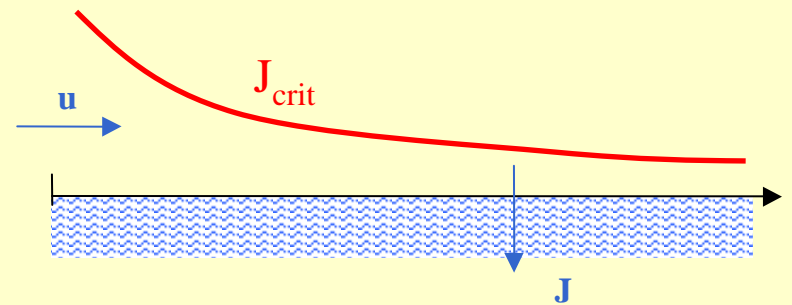
colloidal interaction

$\delta$  : mass boundary layer thickness



**Critical flux distribution**

$$J_{crit} = cste / \delta$$



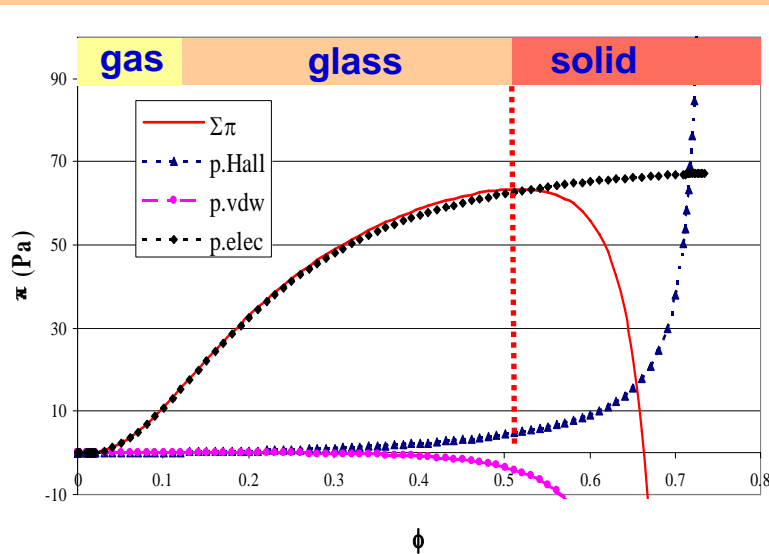
Causes

From causes to consequences

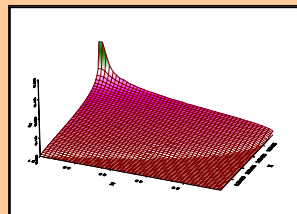
Consequences / Cross flow

## Consequences of $\pi$ behavior on fouling layer formation and structure

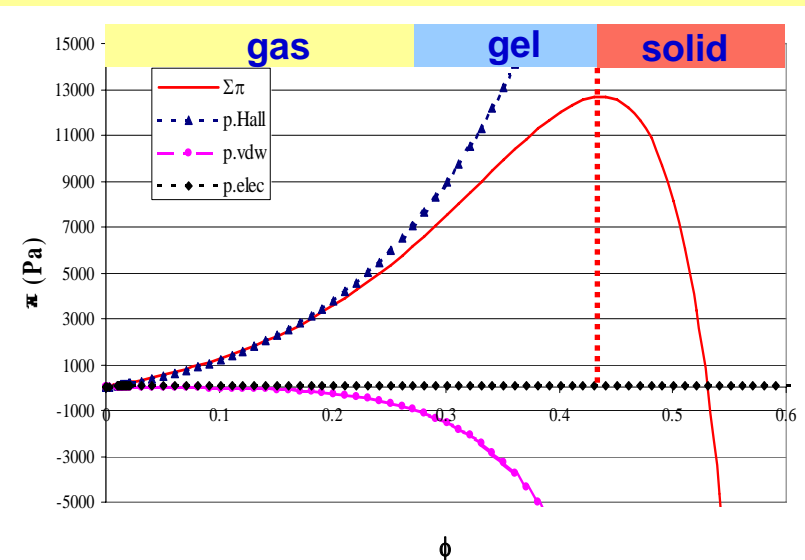
Simulation of **deposit layer** formation with particles



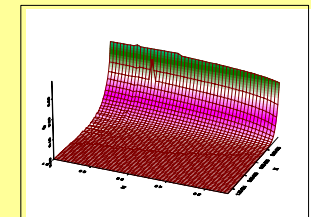
**deposit layer** : stiff formation with progressive development along the membrane



Simulation of **gel layer** formation with macromolecules



**gel layer** : slow formation with rapid development along the membrane

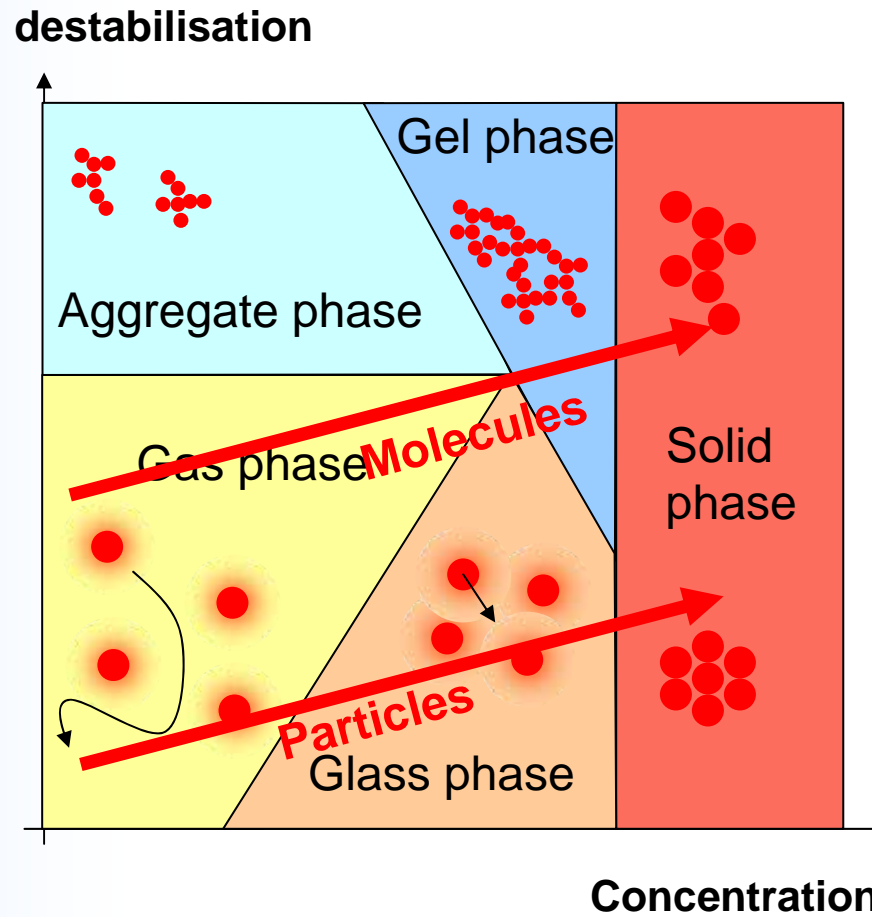


Causes

From causes to consequences

Consequences

## Phase diagram and fouling layer formation and structure



Causes

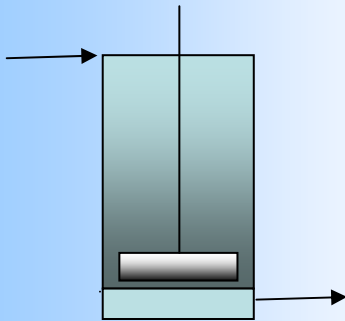
From causes to consequences

Consequences / Dead end

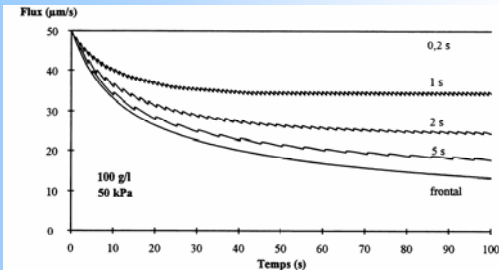
# Experimental highlight of critical accumulated volume fraction

## Principles

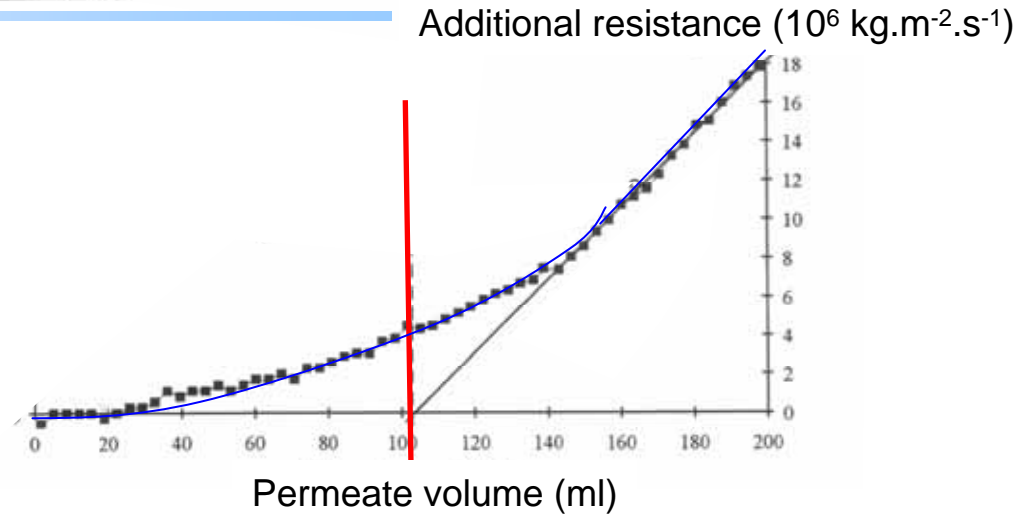
### Dead end



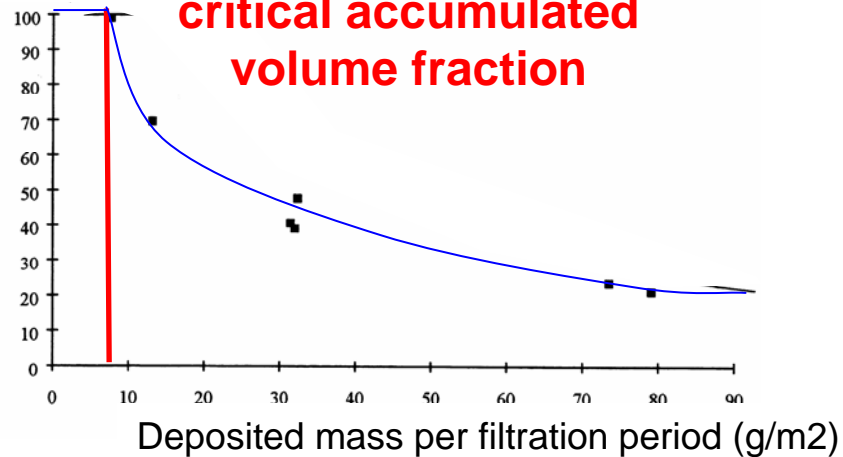
### Sequential dead end filtration



## Results



### Reversibility(%)



Causes

From causes to consequences

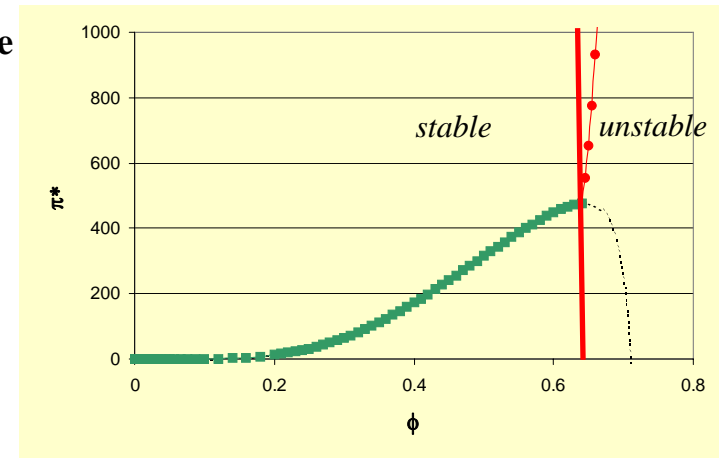
Consequences / Dead end

## Modeling of dead end filtration mode

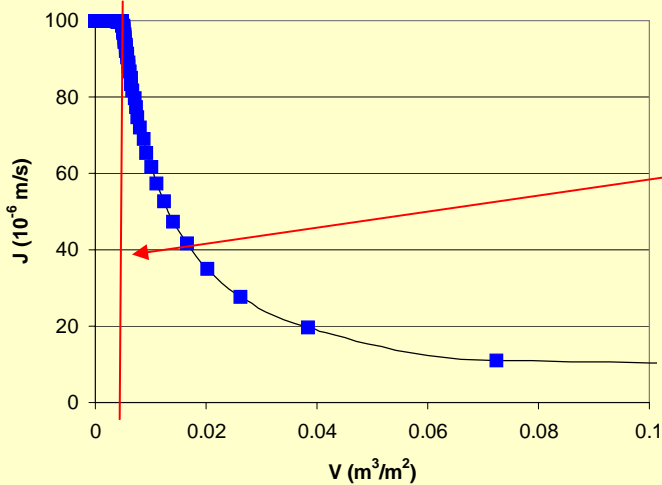
Critical accumulated volume fraction

$$V_{a \text{ crit}} = \frac{D_b}{J} \int_{\pi_b^*}^{\pi_{crit}^*} K(\phi) d\pi^*$$

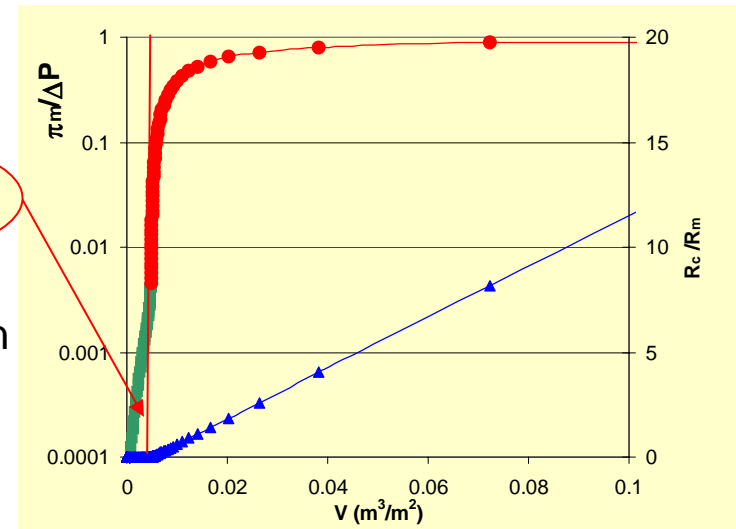
Solid pressure



$a=100 \text{ nm}, \zeta=30 \text{ mV}, I=10^{-4} \text{ M}$



critical filtered volume leading to deposit formation on the surface



Causes

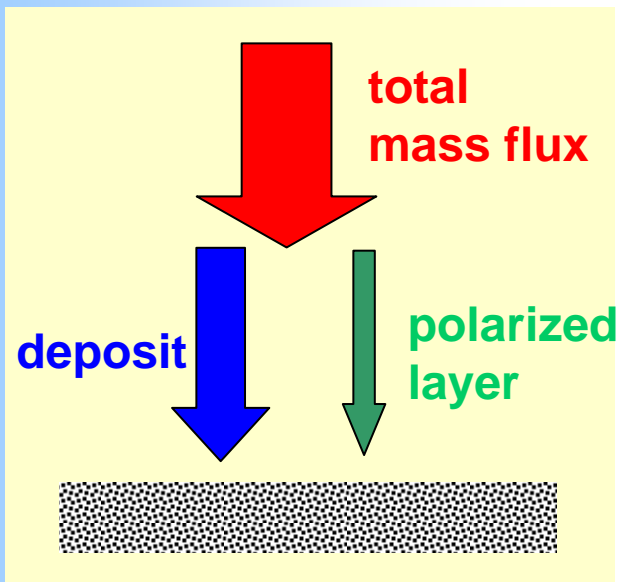
From causes to consequences

Consequences / Dead end

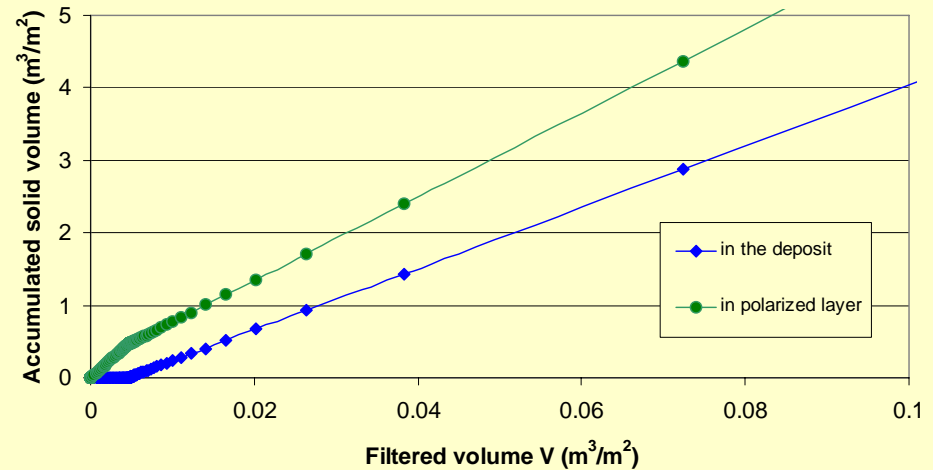
**Critical accumulated volume fraction  
is inversely proportionnal  
to permeate flux**

at given pressure :

critical accumulated volume ↗  
when  
permeate flux (and then time) ↘



**Actual mass of particles irreversibly  
transfer to deposit can be very different  
from the mass transferred by permeation  
from the solution**



**For constant pressure operating mode, specific  
resistance may not be accurately determined  
with classical relationship  $t/V$  versus  $V$  for  
stable suspension**



## Conclusions

**Causes :** spinodal decomposition

**From causes to consequences :**  $\pi$ -based modeling

**Consequences :**

critical flux (or more accurately critical Pe number) in cross flow  
critical accumulated volume fraction in dead end  
formation kinetics and structure of gel or deposit layer

**critical  
fouling  
conditions**

## Questions

- is critical flux a concept for real world membrane processes ?
- is there several critical flux ? i.e. one considering interaction between particles and membrane and another one for particles/particles interactions
- how critical flux has to be experimentally determined ?
- What suspension property can be directly linked to the critical flux (or Peclet number) ?
- Is this concept have future to scale up membrane process ?

## References

- [1] A. Einstein, Investigation on the theory of the Brownian movement, ed. R. Furth, New York : Dover Publications, 1956.
- [2] A.A. Zick and G.M. Homsy, Stokes flow through periodic arrays of spheres, *Journal of fluid mechanics*, 115 (1982) 13-26.
- [3] J.D. Sherwood, Initial and final stages of compressible filtercake compaction, *AIChE J.*, 43 (1997) 1488-1493.
- [4] P. Bacchin, M. Meireles and P. Aimar, Modelling of filtration: From the polarised layer to deposit formation and compaction, *Desalination*, 145 (2002), 139-146.
- [5] P. Bacchin, D. Si-Hassen, V. Starov, M.J. Clifton and P. Aimar, A unifying model for concentration polarization gel-layer formation and particle deposition in cross-flow membrane filtration of colloidal suspensions, *Chem. Eng. Sci.*, 75 (2002) 77-91
- [6] P. Harmant, Contrôle de la structure de dépôts de particules colloïdales en filtration frontale et tangentielle, Thèse de l'Université Paul Sabatier, 2505 (1996)
- [7] P. Bacchin, Formation et résistance au transfert d'un dépôt de colloïdes sur une membrane d'ultrafiltration" Thèse de l'Université Paul Sabatier, Toulouse III, (1994)
- [8] ESPINASSE P., P. BACCHIN, P. AIMAR, Accurate measures of critical flux, a new tool to manage operating conditions in ultrafiltration processes., *Desalination*, 146, 91-97 (2002)
- [9] BACCHIN P. A possible link between critical and limiting flux by consideration of a critical deposit formation along a membrane, to be published on *Journal of Membrane Science*

Causes

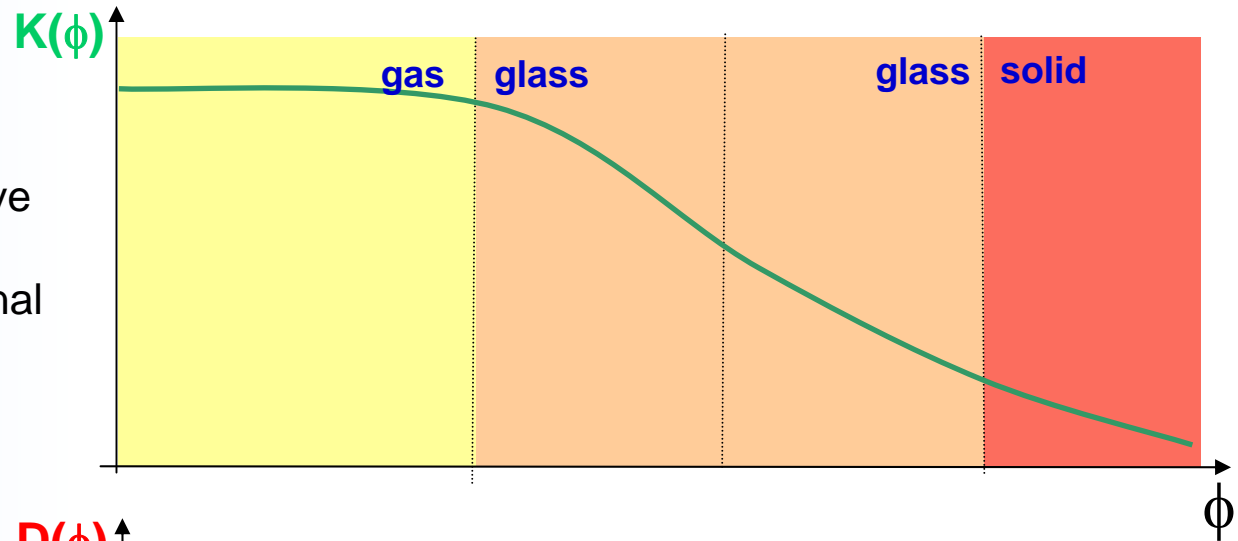
From causes to consequences

Consequences

**Settling coefficient :**

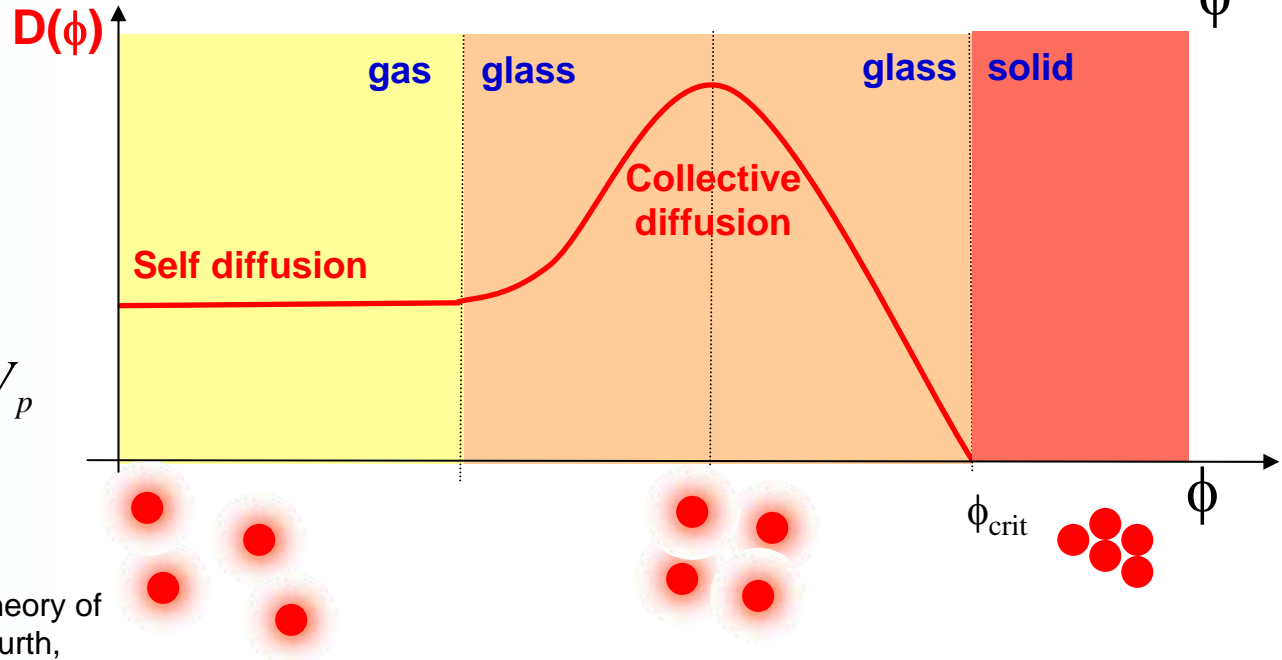
$$K(\phi) = U(\phi) / U_0$$

a dynamic property relative to the resulting velocity particle/water at an external force field

**Diffusion :**

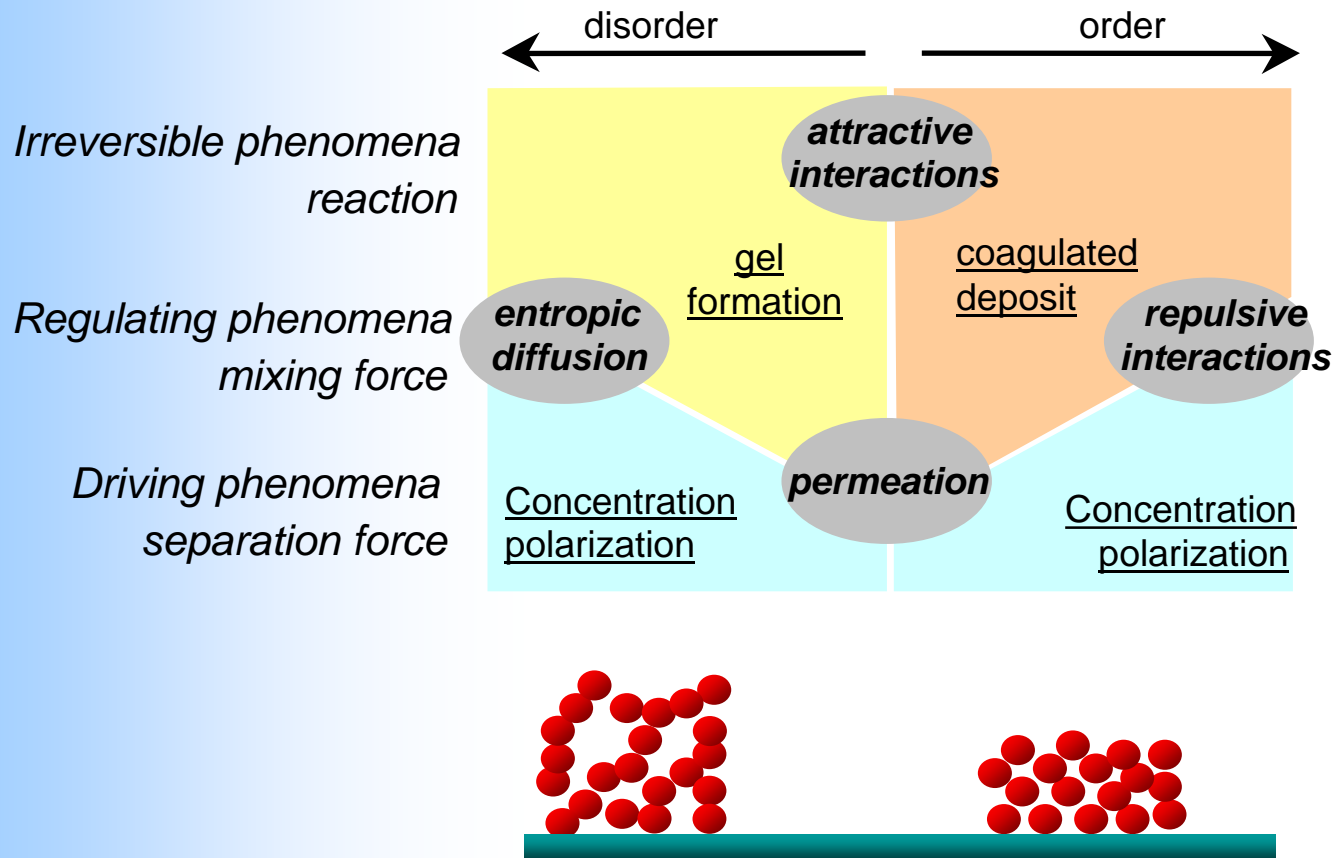
a transfer property relative to particles transport in a concentration gradient

$$D(\phi) = \frac{K(\phi)}{6\pi\mu a} \frac{d\pi}{d\phi} V_p$$

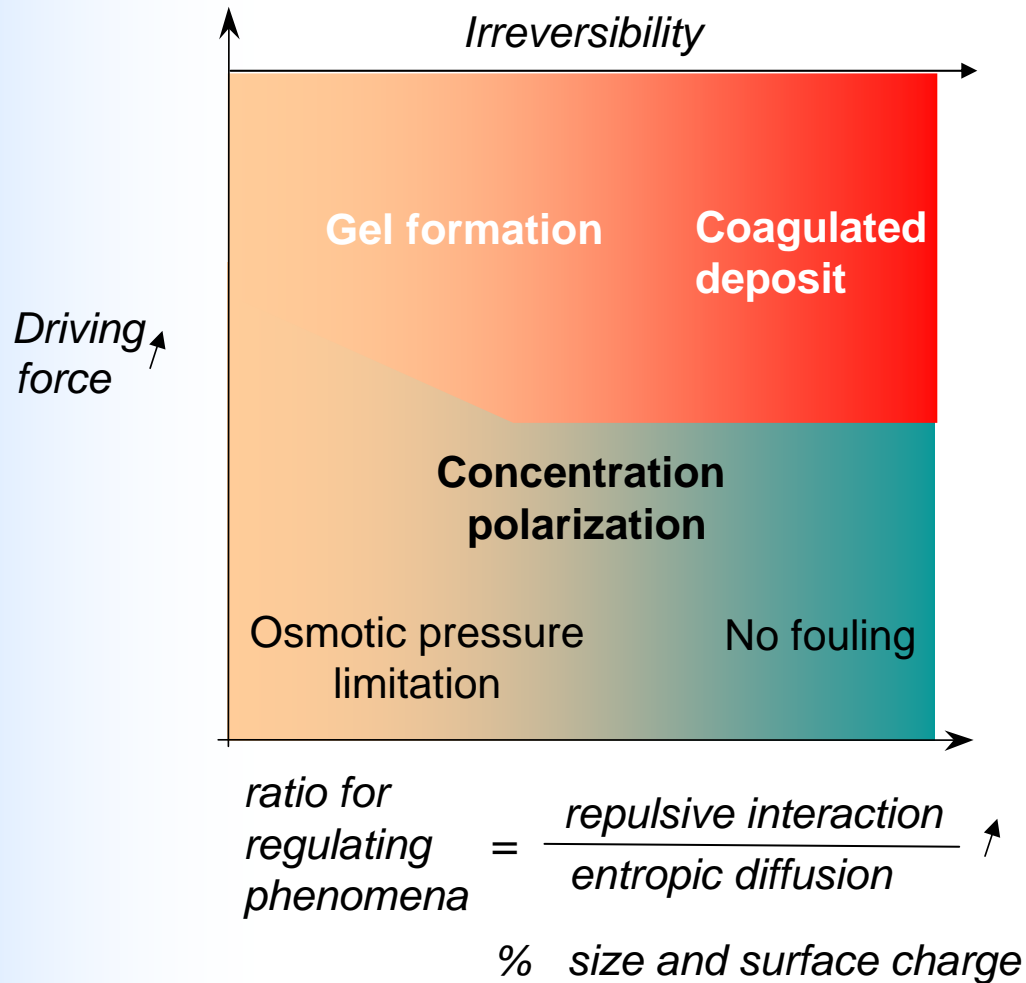


[1] A. Einstein, Investigation on the theory of the Brownian movement, ed. R. Furth, New York : Dover Publications, 1956.

## Osmotic pressure and fouling mechanisms



## Fouling mechanisms and operating conditions



# Conclusions

Osmotic pressure of colloidal suspension is an accessible property depicting the **resistance of the suspension to the local over concentration**

Osmotic pressure use in theoretical modeling leads to interesting simplification and allows to develop **continuous modeling integrating both gel, deposit or polarization mechanisms**

Explanations with  $\pi$ -based modeling are given for :

- critical fouling conditions** : critical flux in cross flow filtration  
critical accumulated mass in dead end
- the effect of physico-chemical properties on fouling layer formation**

**Osmotic pressure and settling coefficient form an indispensable data set to characterize suspension in regard to filtration experiments (or simulation)**

But in which conditions is it sufficient ?

